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# Boron and Nitrogen Doping in Graphene for the Catalysis of Acetylene Hydrochlorination

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**Supporting Information** 

**ABSTRACT:** Exploration of environmentally friendly catalysts is important for acetylene hydrochlorination because the traditional  $HgCl_2$  catalyst is highly toxic and harmful to human health. Herein, boron and nitrogen heteroatoms dually doped on oxide graphene (B,N-G) catalyst were synthesized using a model calcination method and applied as a nonmetallic catalyst for acetylene hydrochlorination. The B,N-G catalyst shows acetylene conversion significantly higher (nearly 95%) than that of singly B- or N-doped graphenes and a little lower than that of Au and Hg catalyst. Density functional theory calculations and temperature-programmed desorption results indicate that the synthetic effect of B and N doping can promote HCl adsorption, which is the rate-



determining step in acetylene hydrochlorination. The excellent catalytic efficiency and relatively low cost of B,N-G makes it a promising catalyst for acetylene hydrochlorination.

**KEYWORDS:** nitrogen and boron doping, graphene, metal-free catalyst, acetylene hydrochlorination, HCl adsorption

# 1. INTRODUCTION

Polyvinyl chloride (PVC) polymerization from vinyl chloride monomer (VCM) is one of the most widely used engineering plastics in various aspects of human life and is suitable for numerous manufacturing various products, such as water pipes and fittings, electric wires, and plastic membranes. The domestic industrial production of VCM in China is mainly throughthe calcium carbide method (acetylene hydrochlorination), and the reaction is catalyzed by carbon-supported mercuric chloride catalyst. However, the toxic mercuric chloride causes serious environmental problems and harm to human health.<sup>1</sup> Therefore, the extended studies on environmentally friendly catalysts have attracted increasing interest and are important for the industrial application of acetylene hydrochlorination.

Considerable catalytic activity has been achieved on some chlorides of transition metals, such as Au,<sup>2</sup> Bi,<sup>3</sup> and Pt,<sup>4</sup> toward acetylene hydrochlorination. Hutchings et al.<sup>5,6</sup> found that Au/AC has the best activity among these transition metals. Hutchings et al. also achieved an optimized catalytic activity when the catalyst contained 1 wt % Au, although the poor stability of a Au catalyst still could not meet the criteria for industrial application.<sup>7–9</sup> Because Au catalysts is expensive and scarce, exploitation of low-cost catalysts may be another development strategy for an acetylene hydrochlorination catalyst.<sup>10,11</sup>

Recently, several N-doped carbon materials have been applied as novel heterogeneous catalysts for acetylene hydrochlorination. In our previous work,<sup>12</sup> we reported that acetylene conversion on g-C<sub>3</sub>N<sub>4</sub>/AC catalyst is ~70% that of a Au/AC catalyst. Wei et al.<sup>13</sup> similarly found that N-doped carbon nanotubes (N-CNTs) enhances the formation of the covalent bond between C<sub>2</sub>H<sub>2</sub> and N-CNTs and therefore promotes the catalytic activity for acetylene hydrochlorination. Recently, Bao et al.<sup>14</sup> reported that a nanocomposite of N-doped carbon derived from silicon carbide (SiC@N–C) directly activates acetylene hydrochlorination; has stable activity during acetylene conversion, which can reach 80%; and has vinyl chloride selectivity >98% at 200 °C. Although N-doped carbon has considerable catalytic activity, its acetylene conversion is still lower than that of Au/AC and Hg/AC catalysts.

In the past few years, N-doped graphene materials have gained substantial attention as catalysts for oxygen reduction reactions (ORRs).<sup>15–19</sup> Studies have reported that by sequentially incorporating N and B into selected sites of the graphene domain enhances the synergistic coupling effect that facilitates the catalytic ORR. In this study, N,B dually doped graphene was prepared through a two-step method, and the obtained catalyst showed a catalytic activity for acetylene hydrochlorination that is only a little lower than that of a Au catalyst.

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Figure 1. TEM images of (a) GO, (b) N-G, and (c) B,N-G.

#### 2. EXPERIMENTAL SECTION

**2.1. Chemicals and Reagents.** Graphite powder (99.85%, J&K Chemical), boric acid ( $H_3BO_3$ , 99.5%, J&K Chemical),  $C_2H_2(gas, 98\%)$ , and HCl (gas,  $\geq$ 99%) were used in the present study.

2.2. Catalyst Preparation. Graphene oxide (GO) was prepared according to the classical Hummers method.<sup>20-22</sup> Graphite powder (5 g) was pretreated by a solution of concentrated H<sub>2</sub>SO<sub>4</sub> (30 mL), K<sub>2</sub>S<sub>2</sub>O<sub>8</sub> (2.5 g), and P<sub>2</sub>O<sub>5</sub> (2.5 g). The preoxidized graphite powder was added into the  $H_2SO_4$ (120 mL) solution and stirred for 10 min in an ice bath, then  $KMnO_4$  (18 g) was added gradually under stirring, and the temperature of the mixture was kept to be below ~15 °C by ice cooling; the mixture was stirred at 35 °C for 2 h. After being diluted with deionized water (250 mL), the mixture was stirred for an additional 2 h. The reaction was cooled to room temperature and poured onto 400 mL of cold, deionized water. Thereafter, 20 mL of fresh 30% H2O2 was added, until observation of the mixture color changed to brilliant yellow along with bubbling, indicating the complete oxidation of the graphite. The resultant solution was centrifuged to obtain the product. The product was washed by 10% HCl aqueous solution and deionized water. The GO powder was collected by lyophilization for further characterizations and experiments.

To prepare the B-doped graphene (B-G), GO powder was mixed with excess boric acid in an  $Al_2O_3$  combustion boat and was heated to 900 °C under flowing Ar for 5 h with a heating rate of 5 °C/min. After annealing, the furnace was cooled to room temperature under the flowing Ar, and then the residual  $B_2O_3$  was removed by washing with boiling water. N-Doped graphene (N-G) was synthesized by annealing GO powder under 20% NH<sub>3</sub>/Ar at 900 °C for 5 h. A two-step B,N codoping of graphene was achieved by annealing the presynthesized B-G intermediate under 20% NH<sub>3</sub>/Ar at 900 °C for 5 h.

**2.3. Catalyst Characterization.** Physical characterization of the sample was performed using a transmission electron microscope (TEM, JEOL, JEM 2010 operating at 200 kV) for its morphological features. X-ray photoelectron spectroscopy (XPS) measurements were performed using an Axis Ultra spectrometer with a monochromatized Al K $\alpha$  X-ray as the excitation source (225W). Temperature-programmed desorption (TPD) was conducted using a Micromeritic ASAP 2720 instrument over a temperature ramp of 50–600 °C, ramp rate of 10 °C/min, and flow rate of 40 mL/min under nitrogen atmosphere. Thermogravimetric analysis (TGA) was conducted with a TGA/DTA system (SDT Q600, TA Instruments, New Castle, Delaware) at room temperature to 900 °C with air

flow of 10 mL/min. The Raman spectra were obtained using a Raman spectrometer (Renishaw) with 514.3 nm Ar laser.

**2.4. Catalytic Performance Evaluation.** The catalyst performance evaluation was performed in a fixed bed microreactor (i.d. = 10 mm). Before initiating the reaction, the reactor was purged with nitrogen to remove water and air in the reaction system. Hydrogen chloride gas was passed through the pipeline at a flow rate of 20 mL/min to activate the catalyst (0.5 g) until the microreactor was heated to 150 °C. Afterward, acetylene and hydrogen chloride were fed through the microreactor, producing a gas hourly space velocity (GHSV,  $C_2H_2$ ) of 36 h<sup>-1</sup>. The exit gas mixture was passed through an absorption bottle containing clean water and injected into a Shimadzu GC-2014C chromatograph for analysis. The conversion of acetylene ( $X_A$ ) and the selectivity to VCM ( $S_{VC}$ ) as the criteria of catalytic performance were defined as the following equations,<sup>9</sup> respectively:

$$X_{\rm A} = \frac{\phi_{\rm A0} - \phi_{\rm A}}{\phi_{\rm A0}} \times 100\%$$
(1)

$$S_{\rm VC} = \frac{\phi_{\rm VC}}{1 - \phi_{\rm A}} \times 100\% \tag{2}$$

In the equations,  $\phi_{A0}$  is defined as the volume fraction of acetylene in the raw gas and  $\phi_A$  is defined as the volume fraction of remaining acetylene in the product gas,  $\phi_{VC}$  is the volume fraction of vinyl chloride in product gas.

The turnover frequency (TOF) of acetylene as the criteria of catalytic performance was calculated using the following equation:

$$TOF = \frac{n_{C_2H_2}}{n_N \times t}$$
(3)

**2.5. Computational Details.** DFT calculations were performed using the hybrid B3LYP<sup>23,24</sup> function, as implemented in the Gaussian 09 computer program package.<sup>25</sup> The standard 6-311G ++\*\* basis set was used for H, C, N, B, and Cl atoms. Atomic charges were calculated using the Mulliken type. The geometries of all structures involved in the mechanism were optimized fully without any restrictions. The frequencies of all geometries were calculated at the same level to identify the nature of the stationary points and obtain the zero-point-energy (ZPE) corrections. All stationary points were characterized as minima (no imaginary frequencies) via Hessian calculation. An important reference point for this calculation is the adsorption energy for HCl on N-G and B,N-G. In this paper, we used the following definitions for adsorption energy.



Figure 2. (a) Raman spectra for GO, N-G, and B,N-G. (b) XPS survey spectra. (c) High-resolution N 1s spectra of B,N-G. (d) High-resolution B 1s spectra of B,N-G.

When HCl is adsorbed on graphene (N-G and B,N-G), the adsorption energy is calculated as

$$E = E_{(\text{system})} - E_{(\text{G})} - E_{(\text{HCl})}$$
(4)

 $E_{\rm (system)}$  is the total energy of the adsorption system,  $E_{\rm (G)}$  denotes the energy of N-G or B,N-G, and  $E_{\rm (HCl)}$  is the energy of HCl, respectively.

#### 3. RESULTS AND DISCUSSION

Figure 1a-c shows the TEM images that display the typical structures and morphologies of GO, N-G, and B,N-G transparent sheets with wrinkled and voile-like features. Despite of the pristine GO with the substitution of several carbon atoms with heteroatoms, the nanosheet morphology was preserved. Figure 2a shows the room temperature Raman spectra for pristine GO, N-G, and B,N-G at 514.3 nm excitation. The  $I_G/I_D$ is a known parameter of carbon materials, which is important in evaluating the degree of graphitization. The G band at 1597 cm<sup>-1</sup> originates from the bond stretching of all sp<sup>2</sup>-bonded pairs, and the D band at 1352 cm<sup>-1</sup> is associated with the sp<sup>3</sup> defect sites. The graphite-induced G-band notably shows a sequential decrease in intensity, which suggests that the increasing presence of N or B heteroatoms in the target is, in fact, bringing about a noticeable change in the ordering degree of the hexagonal lattice. These results are consistent with those of a previous report.  $^{26-28}$ 

The XPS survey spectrum of the elemental compositions of GO, B-G, N-G, and B,N-G shown in Figure 2b presents a predominant C 1s peak (284.5 eV) and an O 1s peak (532.0 eV). The detailed list showing the results of the quantitative evaluations performed through XPS confirms the existence of elemental N and B in the different graphene samples (Table1).

Table 1. Calculated Mass Concentrations of Different Atoms in Various Graphenes  $^a$ 

sample	C, %	O, %	N, %	B, %
GO	65.51	34.48		
B-G	51.73	37.20		11.07
N-G	89.77	4.76	5.47	
N-G (spent)	90.40	4.63	4.97	
B,N-G	55.71	17.86	10.96	15.47
B,N-G (spent)	57.55	17.63	9.59	15.23

"The elemental composition and elemental content of catalysts were determined by XPS method.

Unlike undoped graphene, all the N-doped graphene samples show a visible N 1s peak (399.5 eV). The N levels in N-G and B,N-G are 5.47% and 10.96%, respectively. These results suggest nitrogen can be incorporated in situ into the sp<sup>2</sup> hybridized network in the presence of NH<sub>3</sub>. Similarly, the binding energy values coincide with the data from liter-



**Figure 3.** (a) Catalytic reactivity evaluation of GO, B-G, N-G, and B,N-G. Reactions were carried out at 150 °C, atmospheric pressure, a gas hourly space velocity (GHSV) of 36 h<sup>-1</sup>, and HCl/C<sub>2</sub>H<sub>2</sub> = 1.15/1 (volume ratio). (b) The TOFs for different catalysts: Au/AC, Hg/AC, SiC@N-C, g-C<sub>3</sub>N<sub>4</sub>/AC, B,N-G, and N-G. (c)  $E_{ads}$  of HCl on different types of active sites in N-G and B,N-G. I: The carbon atoms bonded with pyridinic N species. II: The carbon atoms bonded with pyridinic N species. II: The carbon atoms bonded with pyridic N species. III: The carbon atoms bonded with pyridic N species. III: The carbon atoms bonded with pyridic N species. III: The carbon atoms bonded with graphitic N species. Please refer to Figures S3, S4 in the Supporting Information for detailed molecular structures and the calculated HOMO states. (d) TPD profile of GO, N-G, and B,N-G. The samples were preadsorbed by HCl gas for 2 h at a flow rate of 20 mL/min in the microreactor, which was heated to 150 °C. Then it was taken out from the microreactor when the sample was cooled to room temperature. Subsequently, a temperature-programmed desorption TPD was conducted using a Micromeritic ASAP 2720 instrument.

ature.<sup>26,29</sup> The XPS results together with that of Raman spectroscopy strongly confirmed that N and B atoms were successfully introduced into the graphene framework through covalent bonds.

To gain more insight into molecular structure of N/Bbonding configurations, detailed scans for the N 1s and B 1s, including their deconvolutions from high-resolution XPS, are shown in Figure 2c,d. Compared with the N 1s of N-G (Supporting Information, <u>Figure S1</u>), high-resolution N 1s peaks of B,N-G down-shifted to a lower binding energy. The lowest binding energy (398.0 eV) in the N 1s spectrum is related to N–B bonded groups, which means that first with B and then the N can result in boron nitride species. In addition, B,N-G has two split peaks in the high-resolution XPS B 1s spectrum: the main peak at ~188.9 eV is attributable to BC<sub>3</sub>, indicating that B heteroatoms have been successfully incorporated into the graphene lattice network. The B–N chemical bonds have also been observed at 190.9 eV.<sup>30,31</sup>

Under the same reaction conditions, the catalytic activity of GO, B-G, N-G, and B,N-G catalysts were evaluated using a fixed-bed reactor, and the results are shown in Figure 3a. The figure shows that the initial acetylene conversion has the following trend: B,N-G > N-G > B-G > GO. Pristine GO showed negligible acetylene conversion (12.07%), and the acetylene conversion of B-G is only 26.96%, indicating that the B dopant has minimal effect on the catalytic activity on GO. However, N-G displays a substantially higher catalytic activity, and its acetylene conversion reached 62.74%. Numerous literature reports have indicated that N-doped carbon acts as a nonprecious catalyst for acetylene hydrochlorination.<sup>12-14</sup> Li et al. reported that the acetylene conversion of graphitic carbon nitride (g-C<sub>3</sub>N<sub>4</sub>/AC) was ~45% at a GHSV of 50 h<sup>-1</sup>, and the catalytic performance of N-G for acetylene hydrochlorination is similar to those reported in the literature. Dually doped B,N-G catalyst interestingly exhibits an acetylene conversion of 94.98%, indicating that the B atom improves the catalytic

activity of N-G for acetylene hydrochlorination. Supporting Information Figure S2 shows excellent selectivity of the singly/ doubly doped graphenes for vinyl chloride monomers (at more than 98%) throughout the process, and pristine GO had a slightly lower selectivity.

To compare the capacity of chlorinating  $C_2H_2$  into VCM, the turnover frequency (TOF) value of metal-based catalysts (including Au, Hg) as well as the N-G and B,N-G metal-free catalysts are illustrated in Figure 3b. The TOFs of N-G and B,N-G catalysts were  $8.33 \times 10^{-3}$  min<sup>-1</sup> and  $3.32 \times 10^{-2}$  min<sup>-1</sup>, respectively. The TOF of the SiC@N–C catalyst reported by Bao et al. was ~5.63  $\times$  10<sup>-3</sup> min<sup>-1,14</sup> and that of the C<sub>3</sub>N<sub>4</sub> material in our previous work was  $1.42 \times 10^{-2} \text{ min}^{-1.12}$  Those results indicate that the acetylene hydrochlorination rate on B,N-G is somewhat higher than the previous reported catalysts. From Figure 3b, it can also be seen that the TOF of Au/AC and Hg/AC are 5.38 and 0.22 min<sup>-1</sup>, respectively, close to the literature value.<sup>8</sup> It can be concluded the catalytic performance of B,N-G is ~15% of Hg/AC and 6% of Au/AC catalyst. The addition of the second heteroatoms has minimal effect on the selectivity but dramatically enhances the catalytic activity. Both experimental and theoretical studies reveal that the carbon atoms bonded with N species are the active sites, and the schematic illustration of acetylene hydrochlorination for B<sub>1</sub>N-G catalysts is shown in Figure 4, more details of which will be stated later.



Figure 4. Schematic illustration of acetylene hydrochlorination catalyzed by B,N-G catalysts.

The high catalytic activity of the doubly doped graphene layers in the acetylene hydrochlorination can be ascribed to the following two reasons: First, B,N-G provides more active sites compared with N-G because B,N-G has a higher N content than N-G, according to the results shown in Table 1; and second, the presence of the B atom changes the electronic state of the N atom (Supporting Information, <u>Figure S3</u>) and, thus, affects the adsorption of HCl on the N active sites because the adsorption of chloride molecule is the rate-determining step of the acetylene hydrochlorination process.

It is well-known that GO has an abundance of oxygen atoms, so to elucidate the effect of oxygen containing group on the catalytic performance, we built some valid models of GO, N-G, B,N-G with and without the presence of the O atom. The results are listed in <u>Table S1 and Figure S4</u>. These models are based on a previous study about the xygen reduction reaction on a heterodoped graphene.<sup>18,26</sup> From the aforementioned XPS analysis, three N species were considered and investigated because these N species significantly differ in terms of their structures. Different from a traditional Hg and Au catalyst, the

carbon atom acts as the adsorbing site for  $C_2H_2$ , and the nitrogen atom provides the catalytic active site for HCl. Therefore, the carbon atoms bonded with N species are the active sites. As shown in Table S1, the presence of an oxygen atom on N-G and B,N-G catalysts decreases the adsorption of HCl. Because the adsorption of HCl is the rate-determining step of acetylene hydrochlorination, it can be suggested that no obvious promoting effect is present for the oxygen-containing group on the graphene layer.

DFT calculations were also carried out to gain a fundamental understanding of the adsorption of acetylene (Supporting Information, Figure S5). Theoretical results demonstrated that B-doping hardly enhanced the adsorption of acetylene; however, the various N species that interact with HCl have extremely different functions. Different species of N in the catalytic active sites for HCl adsorption  $(E_{ads})$  were identified in Figure 3c. For N-G, a 2-fold coordinated pyridinic N dopant at the edge of the cluster had a specific and dominant HCl adsorption capability. However, no significant HCl adsorption capacity was observed with pyrrolic N, which agrees with the results of previous studies.<sup>12</sup> For dually doped B,N-G, a higher  $E_{ads}$  value than those surveyed for N-G in all three types N was observed, suggesting that the catalyst enhanced the acetylene hydrochlorination reaction and thereby supports the abovediscussed experimental results. The previously identified inactive pyrrolic N atom can boost HCl adsorption because of the coupling interaction between pyridinic N and B, which is shown by the dramatically increasing adsorption energy. The transition of pyrrolic N group from "inactive" into "active" after B incorporation can provide a better catalytic activity compared with N-G for the acetylene hydrochlorination. This result highlights the importance of B in the reaction. As for the graphitic N atom at the center of the graphene layers, the energy of the HCl is minimal; the hydrogen chloride molecule is hardly adsorbed at the active site of graphitic nitrogen. Furthermore, there are no obvious promoting effects between graphitic N and B atom.

Temperature-programmed desorption was performed to directly compare the adsorption and activation of HCl on different graphenes. The desorption temperature in the TPD profiles reflects the binding strength of the adsorbed species with the material surface, and the peak areas correspond to the amount of the adsorbed species. Figure 3d shows that the binding strength of HCl with various graphene materials increases in the following order: GO < N-G < B,N-G. The desorption temperatures of the highest peak were 196.8, 219.2, and 275.5 °C, respectively. In addition, GO has a negligible HCl adsorption ability, implying that almost no catalytic active sites are found on this catalyst. Compared with the original GO without doping, the improvement of the adsorption performance of N-G highly depends on the considerably stronger interaction between N and HCl, thus validating the capability of N to directly activate HCl. A considerable HCl absorption occurred on B,N-G because of additional N content and stronger adsorption of HCl in the presence of B atoms, which explains the excellent acetylene conversion observed. These results support our theoretical observation from DFT calculations of the HCl adsorption and outstanding activity of the B,N-G.

Figure 5 evidently shows that the acetylene conversion of B,N-G decreased from 94.89% to 61.88% within 4 h, indicating its poor catalytic stability during acetylene hydrochlorination. The decrease in activity was due to the severe deactivation of



Figure 5. Conversion of acetylene during 4 h for B,N-G and regenerated B,N-G. Detailed regenerated conditions: hydrogen atmosphere, 10 mL/min, 600  $^{\circ}$ C, 2 h.

catalyst. It was confirmed that the coke formation covering the active sites was the main reason for deactivation, according to the TGA results and as shown in Figure 6. TGA was used to



Figure 6. Thermogravimetric analysis curves recorded in air atmosphere of fresh B,N-G catalyst and spent B,N-G catalyst.

evaluate the degree of carbon deposition on the surface of the catalysts, which was based on previous reported calculation method.<sup>10</sup> In general, there are two parts to the mass loss within 100-500 °C. The first is the burning of coke deposition on the catalyst surface; the second, the oxidation of the carbon carrier in the atmosphere and then escaping as CO<sub>2</sub>. Therefore, the amount of carbon deposition should be equal to the difference between the mass loss of the fresh and used catalysts in the temperature range of 100-500 °C. The mass loss of the spent B,N-G is 5.0 wt % higher than that of the fresh B,N-G catalyst within the 100 to 500 °C. This result indicates that coke deposition occurs on the B,N-G catalyst as the reaction proceeds. Therefore, coke deposition may be the reason for the deactivation of B,N-G in acetylene hydrochlorination. To reactivate the covered active sites, burning off the coke with hydrogen in 600 °C was studied. After the first regeneration, the activity curve implied an initial acetylene conversion recovery to 93%, although the acetylene conversion decreased

rapidly as the reaction went on for 60 min, which demonstrated well its recovery ability. The second regeneration was employed again to recover the activity of the deactivated B,N-G catalyst; however, the initial acetylene conversion partially recovers to 82%, which may be caused by the insufficient regeneration. Overall, burning off the deactivated B,N-G catalyst with hydrogen in 600  $^{\circ}$ C is an available technique in recovering activity.

# 4. CONCLUSIONS

In summary, a B,N-G catalyst was prepared and applied in acetylene hydrochlorination. This catalyst exhibited high activity for acetylene conversion, reaching 94.87%, and is selective to vinyl chloride (above 98%) with GHSV ( $C_2H_2$ ) of 36 h<sup>-1</sup> and at 150 °C. The enhanced catalytic activity of the B,N-G catalyst may be attributed to the improved HCl adsorption, which is proved by the DFT calculation and TPD experiment. Therefore, B,N-G is a promising catalyst for acetylene hydrochlorination because of its high catalytic efficiency and relatively low cost.

#### ASSOCIATED CONTENT

#### Supporting Information

The following file is available free of charge on the ACS Publications website at DOI: 10.1021/acscatal.5b00199.

Adsorption energies of C2H2 and HCl for different catalysts; high-resolution spectra of the catalysts; selectivity of VCM; HOMO states; models of the catalysts; and  $E_{ads}$  of C<sub>2</sub>H<sub>2</sub> on different types of active sites (<u>PDF</u>)

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#### Notes

The authors declare no competing financial interest.

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# REFERENCES

- (1) Li, X.; Zhu, M.; Dai, B. Appl. Catal., B 2013, 142, 234-240.
- (2) Hutchings, G. J.; Haruta, M. Appl. Catal., A 2005, 291, 2-5.
- (3) Smith, D.; Walsh, P.; Slager, T. J. Catal. 1968, 11, 113-130.
- (4) Mitchenko, S. A.; Krasnyakova, T. V.; Mitchenko, R. S.; Korduban, A. N. J. Mol. Catal. A: Chem. **2007**, 275, 101–108.
- (5) Nkosi, B.; Adams, M. D.; Coville, N. J.; Hutchings, G. J. J. Catal. 1991, 128, 378-386.
- (6) Hutchings, G. J. Catal. Today 2002, 72, 11-17.
- (7) Nkosi, B.; Coville, N. J.; Hutchings, G. J.; Adams, M. D.; Friedl, J.; Wagner, F. E. J. Catal. **1991**, 128, 366–377.
- (8) Conte, M.; Carley, A. F.; Heirene, C.; Willock, D. J.; Johnston, P.; Herzing, A. A.; Kiely, C. J.; Hutchings, G. J. *J. Catal.* **2007**, *250*, 231–239.
- (9) Zhang, H.; Dai, B.; Wang, X.; Xu, L.; Zhu, M. J. Ind. Eng. Chem. 2012, 18, 49-54.

(10) Zhang, H.; Dai, B.; Wang, X.; Li, W.; Han, Y.; Gu, J.; Zhang, J. Green Chem. **2013**, *15*, 829–836.

- (11) Huang, C.; Zhu, M.; Kang, L.; Li, X.; Dai, B. Chem. Eng. J. 2014, 242, 69–75.
- (12) Li, X.; Wang, Y.; Kang, L.; Zhu, M.; Dai, B. J. Catal. 2014, 311, 288–294.
- (13) Zhou, K.; Li, B.; Zhang, Q.; Huang, J. Q.; Tian, G. L.; Jia, J. C.; Zhao, M. Q.; Luo, G. H.; Su, D. S.; Wei, F. *ChemSusChem* **2014**, *7*, 723–728.
- (14) Li, X.; Pan, X.; Yu, L.; Ren, P.; Wu, X.; Sun, L.; Jiao, F.; Bao, X. Nat. Commun. 2014, 5, 3688–3694.
- (15) Wang, H.; Maiyalagan, T.; Wang, X. ACS Catal. 2012, 2, 781–794.
- (16) Jiao, Y.; Zheng, Y.; Jaroniec, M.; Qiao, S. Z. J. Am. Chem. Soc. **2014**, 136, 4394–4403.
- (17) Deng, D.; Pan, X.; Yu, L.; Cui, Y.; Jiang, Y.; Qi, J.; Li, W. X.; Fu, Q.; Ma, X.; Xue, Q. Chem. Mater. **2011**, 23, 1188–1193.
- (18) Zhao, Y.; Yang, L.; Chen, S.; Wang, X.; Ma, Y.; Wu, Q.; Jiang, Y.; Qian, W.; Hu, Z. J. Am. Chem. Soc. **2013**, 135, 1201–1204.
- (19) Stankovich, S.; Dikin, D. A.; Dommett, G. H.; Kohlhaas, K. M.; Zimney, E. J.; Stach, E. A.; Piner, R. D.; Nguyen, S. T.; Ruoff, R. S. *Nature* **2006**, 442, 282–286.
- (20) Hummers, W. S., Jr; Offeman, R. E. J. Am. Chem. Soc. 1958, 80, 1339–1339.
- (21) Su, Q.; Pang, S.; Alijani, V.; Li, C.; Feng, X.; Müllen, K. Adv. Mater. 2009, 21, 3191–3195.
- (22) Park, S.; Ruoff, R. S. Nat. Nanotechnol. 2009, 4, 217-224.
- (23) Li, D.; Müller, M. B.; Gilje, S.; Kaner, R. B.; Wallace, G. G. Nat. Nanotechnol. **2008**, *3*, 101–105.
- (24) Becke, A. D. J. Chem. Phys. 1993, 98, 5648-5652.
- (25) Frisch, M. J.; Trucks, G. W.; Schlegel, H. B.; Scuseria, G. E.; Robb, M. A.; Cheeseman, J. R.; Scalmani, G.; Barone, V.; Mennucci, B.; Petersson, G. A.; Nakatsuji, H.; Caricato, M.; Li, X.; Hratchian, H. P.; Izmaylov, A. F.; Bloino, J.; Zheng, G.; Sonnenberg, J. L.; Hada, M.; Ehara, M.; Toyota, K.; Fukuda, R.; Hasegawa, J.; Ishida, M.; Nakajima, T.; Honda, Y.; Kitao, O.; Nakai, H.; Vreven, T.; Montgomery, J. A., Jr.; Peralta, J. E.; Ogliaro, F.; Bearpark, M.; Heyd, J. J.; Brothers, E.; Kudin, K. N.; Staroverov, V. N.; Kobayashi, R.; Normand, J.; Raghavachari, K.; Rendell, A.; Burant, J. C.; Iyengar, S. S.; Tomasi, J.; Cossi, M.; Rega, N.; Millam, N. J.; Klene, M.; Knox, J. E.; Cross, J. B.; Bakken, V.; Adamo, C.; Jaramillo, J.; Gomperts, R.; Stratmann, R. E.; Yazyev, O.; Austin, A. J.; Cammi, R.; Pomelli, C.; Ochterski, J. W.; Martin, R. L.; Morokuma, K.; Zakrzewski, V. G.; Voth, G. A.; Salvador, P.; Dannenberg, J. J.; Dapprich, S.; Daniels, A. D.; Farkas, Ö.; Foresman, J. B.; Ortiz, J. V.; Cioslowski, J.; Fox, D. J. Gaussian 09, Revision C.01; Gaussian, Inc.: Wallingford, CT, 2009.
- (26) Zheng, Y.; Jiao, Y.; Ge, L.; Jaroniec, M.; Qiao, S. Z. Angew. Chem., Int. Ed. 2013, 125, 3192-3198.
- (27) Niyogi, S.; Bekyarova, E.; Itkis, M. E.; Zhang, H.; Shepperd, K.; Hicks, J.; Sprinkle, M.; Berger, C.; Lau, C. N.; Deheer, W. A. *Nano Lett.* **2010**, *10*, 4061–4066.
- (28) Dikin, D. A.; Stankovich, S.; Zimney, E. J.; Piner, R. D.; Dommett, G. H.; Evmenenko, G.; Nguyen, S. T.; Ruoff, R. S. *Nature* **2007**, 448, 457–460.
- (29) Ci, L.; Song, L.; Jin, C.; Jariwala, D.; Wu, D.; Li, Y.; Srivastava, A.; Wang, Z.; Storr, K.; Balicas, L. *Nat. Mater.* **2010**, *9*, 430–435.
- (30) Raymundo-Pinero, E.; Cazorla-Amorós, D.; Linares-Solano, A.; Find, J.; Wild, U.; Schlögl, R. *Carbon* **2002**, *40*, 597–608.
- (31) Park, S.; Hu, Y.; Hwang, J. O.; Lee, E. S.; Casabianca, L. B.; Cai, W.; Potts, J. R.; Ha, H. W.; Chen, S.; Oh, J. *Nat. Commun.* **2012**, *3*, 638–645.